Experimental and modeling study of dihydrogen co-injection in deep aquifers used as UGS to identify key storage parameters



Jean Mura^{1*}, Magali Ranchou-Peyruse^{1,2,3}, Marion Guignard², Marion Ducousso^{1,3}, Pascale Sénéchal⁴, Marie-Pierre Isaure², Peter Moonen⁴, Guilhem Hoareau⁵, Mateus De Souza Buriti¹, Marie Poulain^{1,3}, Anélia Petit⁶, Pierre Chiquet^{3,7}, Guilhem Caumette^{3,8}, Pierre Cézac^{1,3} and Anthony Ranchou-Peyruse^{2,3}

¹ Université de Pau et des Pays de l'Adour, E2S UPPA, LaTEP, Pau, France ² Université de Pau et des Pays de l'Adour, E2S UPPA, CNRS, IPREM, Pau, France ³ Joint Laboratory SEnGA, UPPA-E2S-Teréga, Pau, France ⁴ Université de Pau et des Pays de l'Adour, E2S UPPA, CNRS, DMEX, Pau, France

Background / Objectives

⁵ Université de Pau et des Pays de l'Adour, E2S UPPA, CNRS, TOTAL, LFCR, Pau, France ⁶ STORENGY – Geosciences Department, Bois-Colombes, France

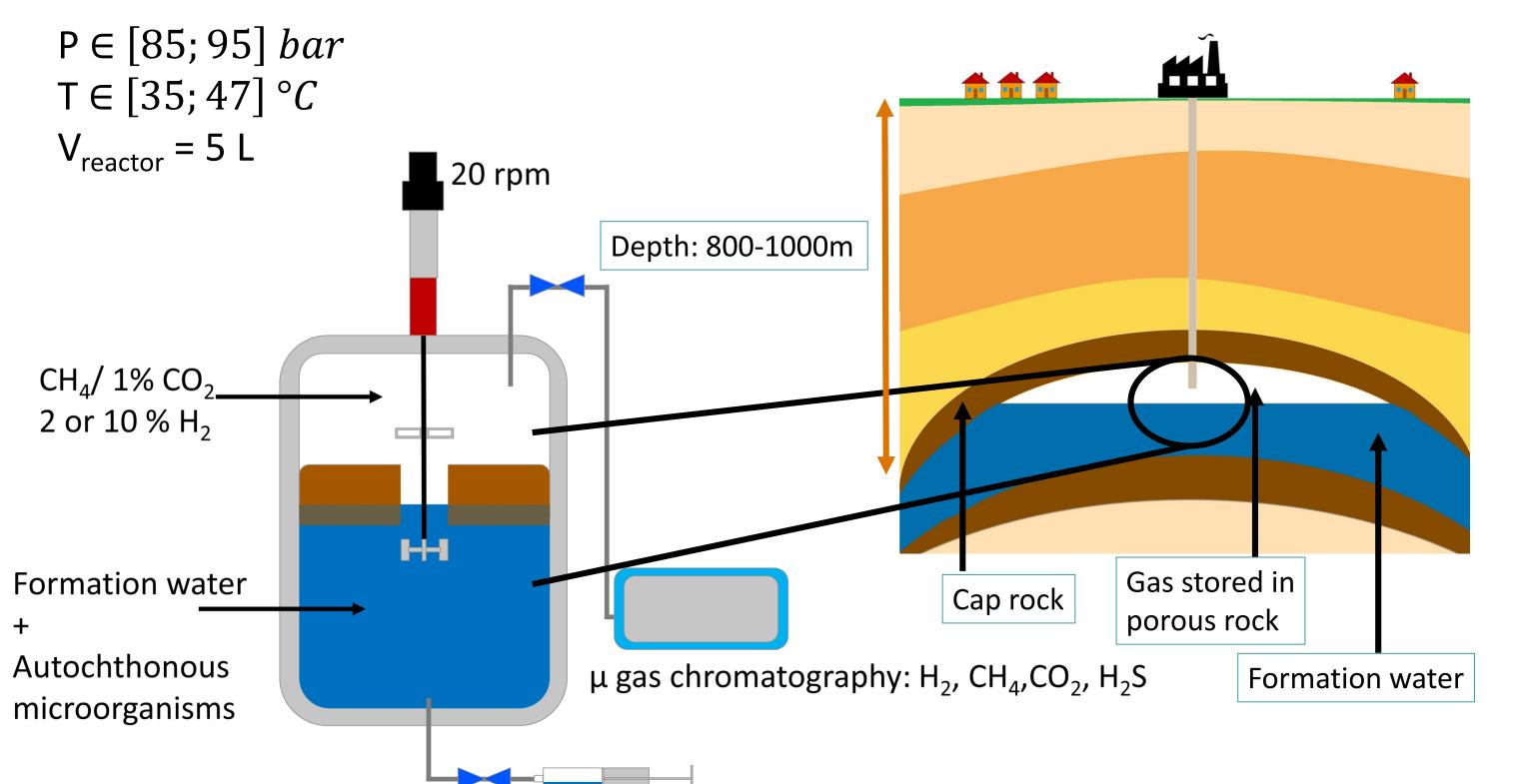
- ⁷ Teréga Geosciences Department, Pau, France
- ⁸ Teréga Environment Department, Pau, France

*Contact: jean.mura@univ-pau.fr

- The European Union aims to produce and import 20 million tons of renewable dihydrogen (H₂) by 2030 as part of it decarbonation strategy [1]. The share of H₂ in natural gas is expected to reach 2%. In many countries in Europe, natural gas storages capacities are mainly represented by underground gas storages (UGS) in deep aquifers (around 1000 m deep).
- H₂ behavior in aquifer still remains uncertain because of its potential consumption by autochthonous hydrogenotrophic microorganisms, the site dependency of these phenomena, and the physico-chemistry of the UGS (sulfate, carbonates, temperature, etc.).
- Pilot experiments and modeling are needed to gather data and extrapolate results to the aquifer scale

Experimental setup

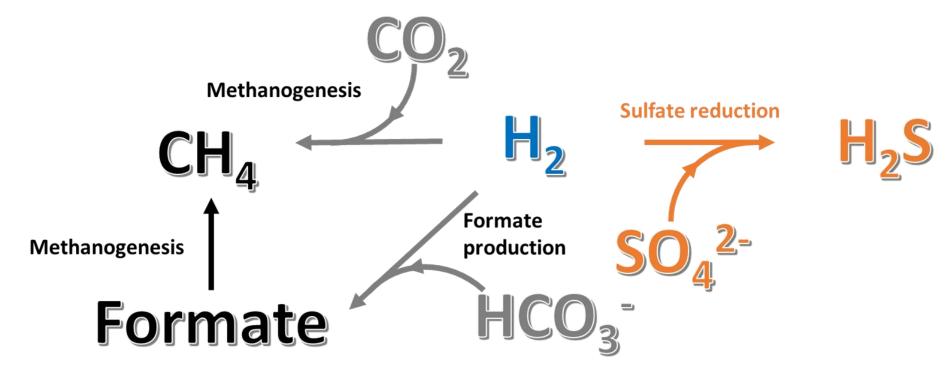
3 aquifers simulated in a high-pressure reactor [2,3]



Ionic chromatography / ICP: Acetate, Formate, SO₄²⁻, HCO₃⁻, Ca²⁺, Mg²⁺, Fe, Ba Reactor in situ pH/Eh calculated using a hybrid experimental/modeling protocol Taxonomic Diversity

Modeling approach

OD dynamic model of the reactor with PHREEQC v3



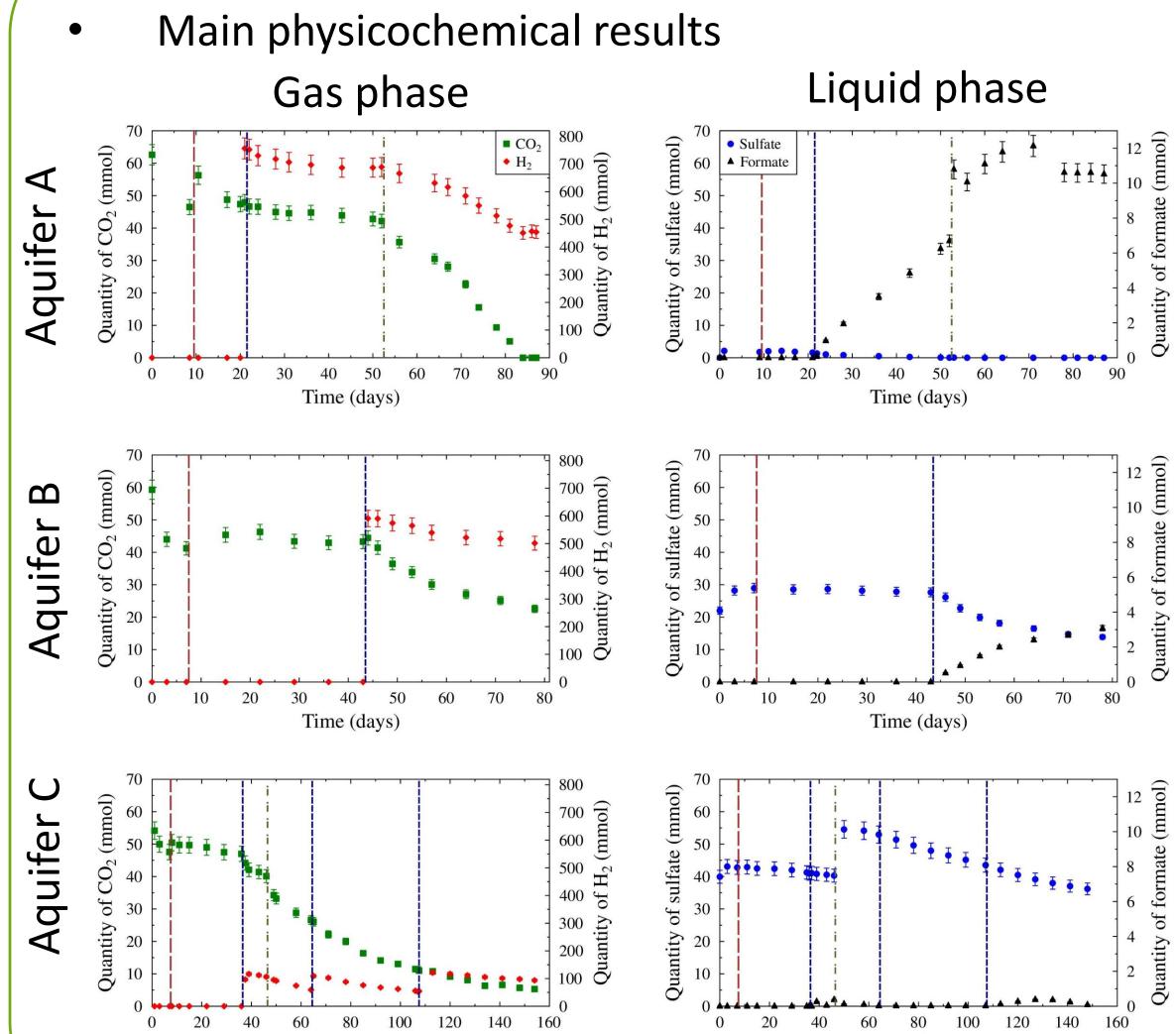
Thermoddem database

(mol.kg⁻¹), D: death rate function (s⁻¹)

- Liquid vapor equilibrium (Peng Robinson equation of state)
- Mineral dissolution/precipitation
- Microbial population evolution and respiration rate:
 - Biochemical equation of growth:

 $HCO_{3(aq)}^{-} + 2,1H_{2(aq)} + 0,2NH_{4(aq)}^{+} + 0,8H_{(aq)}^{+} \rightarrow CH_{1,8}O_{0.5}N_{0.2} + 2,5H_2O_{(l)}$ Kinetic law of growth and death Theoretical composition of a cell (noted B) dB $\frac{1}{dt} = \mu_{max} F_{inhib}(S, pH, \dots)B - DB$ With B : Biomass (mol.kg⁻¹), μ_{max} : growth rate in ideal conditions (s⁻¹), F_{inhib} : inhibition factor, S: substrate

Results



- Sulfate reduction happened in all experiments but didn't always lead to total sulfate consumption.
- When presents, methanogens activity was inhibited during sulfate reduction.
- Inhibition of methanogenesis and formate production by alkaline pH was observed while HCO₃⁻ and H₂ remained.
- Inhibition of sulfate reduction by lack of nutrients such as nitrogen or phosphorus is hypothesized.
- Attenuation of produced H₂S occurred, probably through iron-sulfide precipitation and adsorption (on the solid and on the reactor walls).
- Global impact on the rock was estimated to be minor, but precipitation/dissolution
- Example of modeling results for aquifer A Experimental — Model 0.0 (%) (%) 0.4 CO2 H2 0.2 Methanogenesis (cell/m (cell/ml 10⁶ 106 104 S 10^{4} Cer redu 10² 10² (mmol/kg) (mmol/kg) Formate 0.8 production Sulfate reduction 0.6 Ite 0.4 Sulfate Methanogenesis 0.2 iol/kg) iol/kg) 2.5 1.5 2.0 um) 1.0 1.5 1.0 0.5 Mg² Ca² Calcite/Dolomite precipitation Dolomite precipitation 0.5

Teréga storengy

engie

Time (days) Time (days)	Time (days)Time (days) $$ CH4-CO2 reinjection $$ H2 injection $$ Formation wate	r injection reactions are still expected.	0.0 + + + + + + + + + + + + + + + + + +	0.0 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1
-------------------------	---	---	---	---

Conclusion / Perspectives

- Aquifers with low electron acceptors (especially sulfate), nutrients availability, and pH buffering species (such as CO₂) should be favored to decrease H₂ loss and H₂S production.
- H₂ consumption could cease after an initial loss due to inhibition processes or due to the total consumption of electron acceptors. \bullet
- The model developed in this study should be coupled with large scale experiments to calibrate reservoir simulations in the aim of anticipating the extent of biogeochemical reactions at the aquifer scale.

IPREM

nstitut des sciences analytiques

References

[1] European Commission. Hydrogen. Available at: https://energy.ec.europa.eu/topics/energy-systems-integration/hydrogen_en (Accessed May 15, 2024); [2] Haddad et al. (2022) Energy Environ. Sci., vol. 15, no. 8, pp. 3400–3415, doi: 10.1039/D2EE00765G; [3] J. Mura et al. (2024) Int. J. Hydrog. Energy, vol. 63, pp. 330–345, Apr. 2024, doi: 10.1016/j.ijhydene.2024.02.322.