

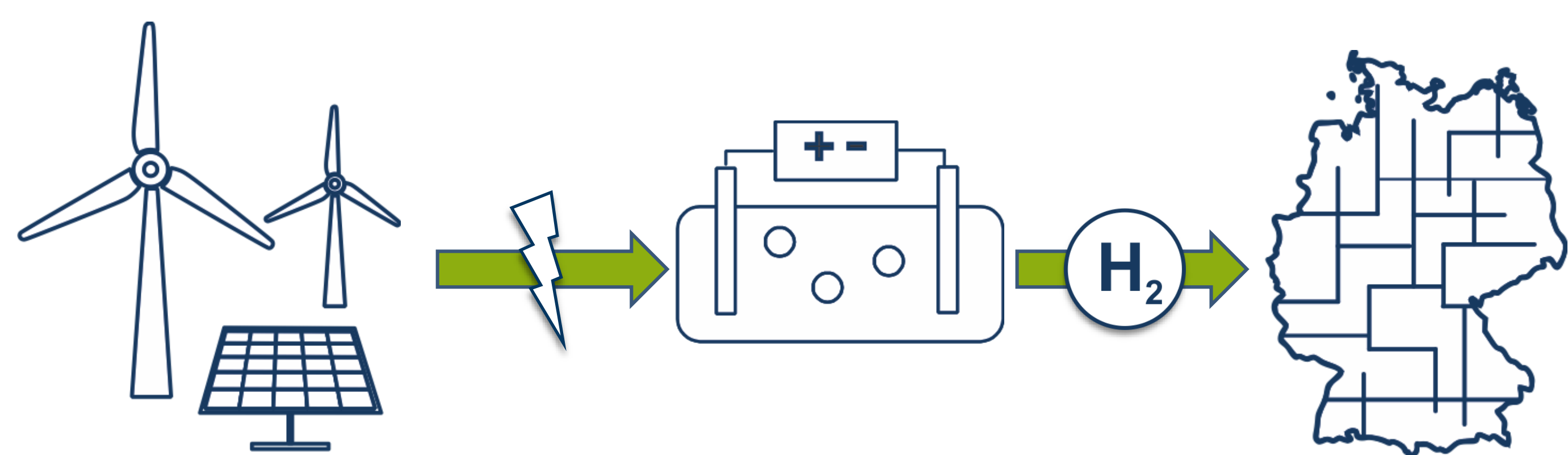
NEW FUNDAMENTAL EQUATIONS OF STATE FOR AN IMPROVED DESCRIPTION OF HYDROGEN-RICH MIXTURES WITH THE REFERENCE MODEL GERG-2008

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MOTIVATION

- The production of green hydrogen from renewable energies by electrolysis is considered a promising technology for the decarbonization and flexibilization of our energy supply
- The injection of green hydrogen into the natural gas grid allows for a step-by-step substitution of the fossil energy carrier natural gas using the existing infrastructure for distribution and storage of the gas mixture
- The changes in thermodynamic properties resulting from an increased hydrogen injection have to be considered to ensure a safe and efficient operation of the gas grid, gas storage facilities, conversion technologies and a variety of other technical processes
- Optimization of the reference model GERG-2008¹ regarding the description of hydrogen-rich natural gas properties in a wide range of temperature, pressure, and composition is required
- New equations of state for 20 binary hydrogen mixtures are needed



FUNDAMENTAL EQUATIONS OF STATE FOR MIXTURES

- Equations of state are formulated in terms of the reduced Helmholtz energy α as a function of temperature T , density ρ , and composition \bar{x}

$$\alpha(\delta, \tau, \bar{x}) = \frac{a(\rho, T, \bar{x})}{RT} = \alpha^o(\rho, T, \bar{x}) + \alpha^r(\delta, \tau, \bar{x})$$

- The ideal part $\alpha^o(\rho, T, \bar{x})$ describes the mixture behavior of the involved pure components in the reference state of the ideal-gas

$$\alpha^o(\rho, T, \bar{x}) = \sum_{i=1}^N x_i [\alpha_{o,i}^o(\delta_{o,i}, \tau_{o,i}) + \ln x_i]$$

- The residual part $\alpha^r(\delta, \tau, \bar{x})$ considers the molecular interactions of the real fluid

$$\alpha^r(\delta, \tau, \bar{x}) = \sum_{i=1}^N x_i \alpha_{o,i}^r(\delta, \tau) + \sum_{i=1}^{N-1} \sum_{j=i+1}^N x_i x_j F_{ij} \alpha_{ij}^r(\delta, \tau)$$

- The reduced density δ and the reciprocal reduced temperature τ are determined with composition-dependent reducing functions

$$\delta = \frac{\rho}{\rho_r(\bar{x}, \rho_{c,i}, \beta_{v,ij}, \gamma_{v,ij})} \quad \tau = \frac{T_r(\bar{x}, T_{c,i}, \beta_{T,ij}, \gamma_{T,ij})}{T}$$

- Non-ideal mixture behavior is modelled with a binary-specific departure function

$$\alpha_{ij}^r(\delta, \tau) = \sum_{k=1}^{K_{pol}} n_k \tau^{t_k} \delta^{d_k} + \sum_{k=K_{pol}+1}^{K_{pol}+K_{exp}} n_k \tau^{t_k} \delta^{d_k} e^{-\delta^{l_k}} + \sum_{k=K_{pol}+K_{exp}+1}^{K_{pol}+K_{exp}+K_{GBS}} n_k \tau^{t_k} \delta^{d_k} e^{-[\eta_k(\delta-\varepsilon_k)^2 - \beta_k(\tau-\gamma_k)^2]}$$

- The adjustable parameters are fitted to experimental data using a non-linear algorithm²

RESULTS

DESCRIPTION OF THE HOMOGENEOUS REGION

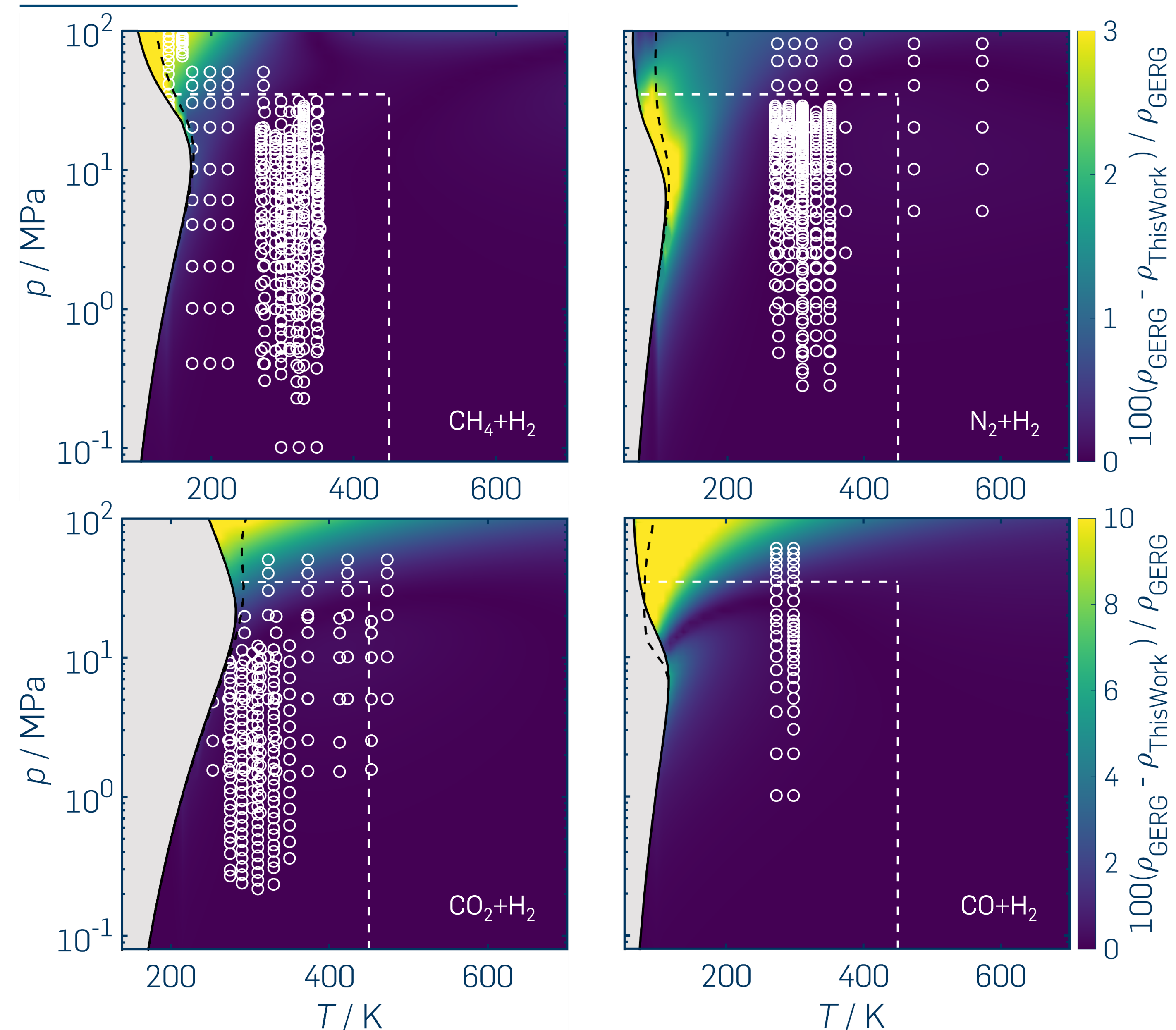


Fig. 1: Percentage deviation in density in the homogeneous region between the new models and GERG-2008¹ at equimolar composition. The white dashed lines represent the normal range of validity of both models and the black dashed lines mark the phase boundary calculated with the GERG-2008.¹ The circles represent the available experimental density data at approximately equimolar compositions.

DESCRIPTION OF THE PHASE EQUILIBRIUM

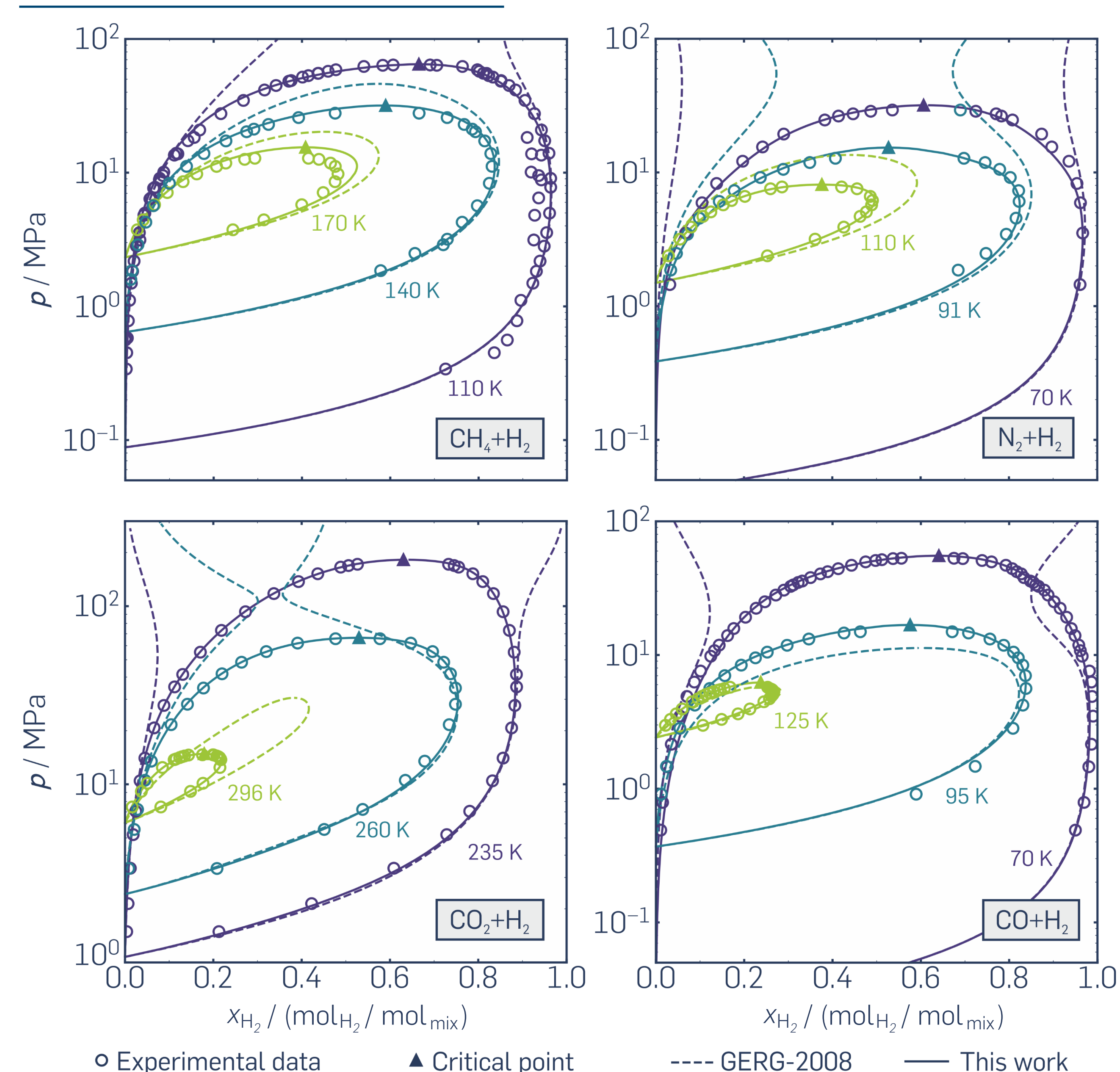


Fig. 2: p, x -diagrams of the binary mixtures at selected temperatures calculated with the new models and the GERG-2008¹ compared to experimental phase equilibrium data.

REFERENCES

- Kunz, O., & Wagner, W., Journal of Chemical & Engineering Data, 57(11), 3032-3091 (2012)
- Lemmon, E. W. & Jacobsen, R. T., Journal of Physical and Chemical Reference Data, 34(1), 69-108 (2005)